

Table 2

<b>Matting Agent</b>	<b>Composition</b>	<b>Median Diameter of Particle (microns)</b>	<b>95<sup>th</sup> Percentile* (microns)</b>
1	Alkali alumina silica	4	10
2	Alkali alumina silica	4	18
3	Alkali alumina silica	8	30

\* Particle Diameter for which 95% of particles are smaller.

Table 3.

<b>Film Sample</b>	<b>Gloss (60 degrees)</b>	<b>Roughness Ranking (1= low roughness, 5= high roughness)</b>
Example 1	16	4
Example 2	22	4
Example 3	19	3
Example 4	19	1
Example 5	26	1

What is claimed is:

1. A thermoplastic article having a matte, printable surface comprising from 15 to 30 percent  
5 by weight of inorganic particles.
2. The thermoplastic article of claim 1 wherein said thermoplastic is selected from the group  
consisting of ABS terpolymer, ASA copolymer, polycarbonate, polyester, PETG, MBS copolymer,  
HIPS, acrylonitrile/acrylate copolymer, polystyrene, SAN, MMA/S, an acrylonitrile/methyl  
10 methacrylate copolymer, impact modified polyolefins, PVC, impact modified PVC, imidized acrylic  
polymer, fluoropolymers, polyvinylidenedifluoride (PVDF), PVDF-acrylic polymer blends, acrylic  
polymer or impact modified acrylic polymer
3. The thermoplastic article of claim 2 wherein said thermoplastic is a polymethylmethacrylate  
15 homopolymer or copolymer.
4. The thermoplastic article of claim 1 wherein said inorganic particles are selected from the  
group consisting of silica, talc, alumina, metal carbonates, or mixtures thereof.
- 20 5. The thermoplastic article of claim 1 wherein said inorganic particles are alkali alumina silica.
6. The thermoplastic article of claim 1 wherein said inorganic particles have a mean particle size  
of from 2 to 20.
- 25 7. The thermoplastic article of claim 1 wherein said inorganic particles have a mean particle size  
of from 2 to 12.
8. The thermoplastic article of claim 1 wherein said inorganic particles have a mean particle size  
of from 3 to 8.

## **ABSTRACT**

This invention relates to thermoplastic articles having printable matte surfaces. The printable matte surface is achieved by blending inorganic particles, and especially silica particles, having a mean particle size of from 2 to 30 micron and a narrow particle size distribution into the thermoplastic at from 15 to 30 percent by weight.

Docket No.  
IR 3746 NP

# Declaration and Power of Attorney For Patent Application

## English Language Declaration

As a below named inventor, I hereby declare that:

My residence, post office address and citizenship are as stated below next to my name,

I believe I am the original, first and sole inventor (if only one name is listed below) or an original, first and joint inventor (if plural names are listed below) of the subject matter which is claimed and for which a patent is sought on the invention entitled

**THERMOPLASTIC ARTICLE WITH A PRINTABLE MATTE SURFACE**

the specification of which

(check one)

☒ is attached hereto.

☐ was filed on \_\_\_\_\_ as United States Application No. or PCT International  
Application Number \_\_\_\_\_  
and was amended on \_\_\_\_\_  
(if applicable)

I hereby state that I have reviewed and understand the contents of the above identified specification, including the claims, as amended by any amendment referred to above.

I acknowledge the duty to disclose information which is material to patentability as defined in 37 CFR 1.56, including for continuation-in-part applications, material information which became available between the filing date of the prior application and the national or PCT international filing date of the continuation-in-part application.

I hereby claim foreign priority benefits under 35 U.S.C. 119(a)-(d) or (f), or 365(b) of any foreign application(s) for patent, or plant breeder's rights certificate(s), or 365(a) of any PCT International application which designated at least one country other than the United States of America, listed below and have also identified below, by checking the box, any foreign application for patent, inventor's or plant breeder's rights certificate(s), or any PCT international application having a filing date before that of the application on which priority is claimed.

### Prior Foreign Application(s)

### Priority Claimed

_____ (Number)	_____ (Country)	_____ (Day/Month/Year Filed)
_____ (Number)	_____ (Country)	_____ (Day/Month/Year Filed)
_____ (Number)	_____ (Country)	_____ (Day/Month/Year Filed)

☐  
☐  
☐

(Application Serial No.)

(Filing Date)

(Application Serial No.)

(Filing Date)

(Application Serial No.)

(Filing Date)

I hereby claim the benefit under 35 U. S. C. Section 120 of any United States application(s), or Section 365(c) of any PCT International application designating the United States, listed below and, insofar as the subject matter of each of the claims of this application is not disclosed in the prior United States or PCT International application in the manner provided by the first paragraph of 35 U.S.C. Section 112, I acknowledge the duty to disclose to the United States Patent and Trademark Office all information known to me to be material to patentability as defined in Title 37, C. F. R., Section 1.56 which became available between the filing date of the prior application and the national or PCT International filing date of this application:

(Application Serial No.)

(Filing Date)

(Status)  
(patented, pending, abandoned)

(Application Serial No.)

(Filing Date)

(Status)  
(patented, pending, abandoned)

(Application Serial No.)

(Filing Date)

(Status)  
(patented, pending, abandoned)

(Application Serial No.)

(Filing Date)

(Status)  
(patented, pending, abandoned)

(Application Serial No.)

(Filing Date)

(Status)  
(patented, pending, abandoned)

(Application Serial No.)

(Filing Date)

(Status)  
(patented, pending, abandoned)

I hereby declare that all statements made herein of my own knowledge are true and that all statements made on information and belief are believed to be true; and further that these statements were made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both, under Section 1001 of Title 18 of the United States Code and that such willful false statements may jeopardize the validity of the application or any patent issued thereon.

**POWER OF ATTORNEY:** As a named inventor, I hereby appoint the following attorney(s) and/or agent(s) to prosecute this application and transact all business in the Patent and Trademark Office connected therewith. *(list name and registration number)*

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Second inventor's signature	Date
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Citizenship	
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PATENT APPLICATION SERIAL NO. \_\_\_\_\_

U.S. DEPARTMENT OF COMMERCE  
PATENT AND TRADEMARK OFFICE  
FEE RECORD SHEET

05/11/2005 CNGUYEN2 00000004 012717 11123539

01 FC:1011	300.00 DA
02 FC:1111	500.00 DA
03 FC:1311	200.00 DA

PTO-1556  
(5/87)

**PATENT APPLICATION FEE DETERMINATION RECORD**  
Effective December 8, 2004

11123 539

**CLAIMS AS FILED - PART I**

	(Column 1)	(Column 2)
TOTAL CLAIMS	8	
FOR	NUMBER FILED	NUMBER EXTRA
TOTAL CHARGEABLE CLAIMS	8 minus 20 =	0
INDEPENDENT CLAIMS	1 minus 3 =	0
MULTIPLE DEPENDENT CLAIM PRESENT <input type="checkbox"/>		

\* If the difference in column 1 is less than zero, enter "0" in column 2

SMALL ENTITY TYPE ☐

OR ☒ OTHER THAN SMALL ENTITY

RATE	FEE
BASIC FEE	150.00
X\$ 25=	
X100=	
+180=	
TOTAL	

RATE	FEE
BASIC FEE	300.00
X\$50=	
X200=	
+360=	
TOTAL	300

**CLAIMS AS AMENDED - PART II**

	(Column 1)	(Column 2)	(Column 3)
AMENDMENT A	CLAIMS REMAINING AFTER AMENDMENT	HIGHEST NUMBER PREVIOUSLY PAID FOR	PRESENT EXTRA
	Total	0 Minus	00 =
	Independent	0 Minus	000 =
	FIRST PRESENTATION OF MULTIPLE DEPENDENT CLAIM <input type="checkbox"/>		

SMALL ENTITY OR

OTHER THAN SMALL ENTITY

RATE	ADDITIONAL FEE
X\$ 25=	
X100=	
+180=	
TOTAL ADDIT. FEE	

RATE	ADDITIONAL FEE
X\$50=	
X200=	
+360=	
TOTAL ADDIT. FEE	

	(Column 1)	(Column 2)	(Column 3)
AMENDMENT B	CLAIMS REMAINING AFTER AMENDMENT	HIGHEST NUMBER PREVIOUSLY PAID FOR	PRESENT EXTRA
	Total	0 Minus	00 =
	Independent	0 Minus	000 =
	FIRST PRESENTATION OF MULTIPLE DEPENDENT CLAIM <input type="checkbox"/>		

RATE	ADDITIONAL FEE
X\$ 25=	
X100=	
+180=	
TOTAL ADDIT. FEE	

RATE	ADDITIONAL FEE
X\$50=	
X200=	
+360=	
TOTAL ADDIT. FEE	

	(Column 1)	(Column 2)	(Column 3)
AMENDMENT C	CLAIMS REMAINING AFTER AMENDMENT	HIGHEST NUMBER PREVIOUSLY PAID FOR	PRESENT EXTRA
	Total	0 Minus	00 =
	Independent	0 Minus	000 =
	FIRST PRESENTATION OF MULTIPLE DEPENDENT CLAIM <input type="checkbox"/>		

RATE	ADDITIONAL FEE
X\$ 25=	
X100=	
+180=	
TOTAL ADDIT. FEE	

RATE	ADDITIONAL FEE
X\$50=	
X200=	
+360=	
TOTAL ADDIT. FEE	

\* If the entry in column 1 is less than the entry in column 2, write "0" in column 3.  
 \* If the "Highest Number Previously Paid For" IN THIS SPACE is less than 20, enter "20."  
 \* If the "Highest Number Previously Paid For" IN THIS SPACE is less than 3, enter "3."

The "Highest Number Previously Paid For" (Total or Independent) is the highest number found in the appropriate box in column 1.



PATENT

Attorney Docket No. IR 3746 NP

**IN THE UNITED STATES PATENT AND TRADEMARK OFFICE**

Applicant: EDGECOMBE, Brian

Group Art Unit: n/a

Serial No.: Not yet assigned

Examiner: Not yet assigned

Filing Date: Herewith

For: **THERMOPLASTIC ARTICLE WITH A PRINTABLE MATTE  
SURFACE**

**INFORMATION DISCLOSURE STATEMENT**

Commissioner for Patents  
P.O. Box 1450  
Alexandria, VA 22313-1450

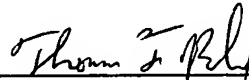
Sir:

Applicant submits herewith a copy of the documents listed on the attached

Form PTO-1449.

Respectfully submitted,

Date: May 6, 2005



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Encls.

<b>INFORMATION DISCLOSURE CITATION</b> <i>(Use several sheets if necessary)</i>				Docket Number (Optional) <b>IR 3746 NP</b>		Application Number <b>Not yet assigned</b>		
				Applicant(s) <b>EDGECOMBE, Brian</b>				
				Filing Date <b>Herewith</b>		Group Art Unit <b>Not yet assigned</b>		
<b>U.S. PATENT DOCUMENTS</b>								
*EXAMINER INITIAL	REF	DOCUMENT NUMBER	DATE	NAME	CLASS	SUBCLASS	FILING DATE IF APPROPRIATE	
	1.	US 4,906,676	06MAR90	IDA, Kozo				
	2.	US 5,346,954	13SEP84	WU, J. et al				
	3.	US 6,524,694	25FEB03	PHILLIPS, Tracy				
<b>U.S. PATENT APPLICATION PUBLICATIONS</b>								
*EXAMINER INITIAL	REF	DOCUMENT NUMBER	DATE	NAME	CLASS	SUBCLASS	FILING DATE IF APPROPRIATE	
	1.	US 2003/0175499	18SEP03	PHILLIPS, Tracy				
<b>FOREIGN PATENT DOCUMENTS</b>								
	REF	DOCUMENT NUMBER	DATE	COUNTRY	CLASS	SUBCLASS	Translation	
							YES	NO
	1.	EP 1022115	20JAN01	EP			✓	
	2.	JP 2001/081266	27MAR01	JP				✓
<b>OTHER DOCUMENTS</b> <i>(Including Author, Title, Date, Pertinent Pages, Etc.)</i>								
EXAMINER				DATE CONSIDERED				
<b>EXAMINER:</b> Initial if citation considered, whether or not citation is in conformance with MPEP Section 609; Draw line through citation if not in conformance and not considered. Include copy of this form with next communication to applicant.								

(19)



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**EP 1 022 115 B1**

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(22) Date of filing: 20.01.2000

### (54) Polymeric articles having a textured surface and frosted appearance

Polymere Gegenstände mit strukturierter Oberfläche und mattem Aussehen

Articles polymères ayant une surface texturée et un aspect mat

(84) Designated Contracting States:  
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MC NL PT SE

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(56) References cited:  
EP-A- 0 596 290 EP-A- 0 786 494  
WO-A-97/14749 GB-A- 2 220 002  
US-A- 3 345 434 US-A- 3 883 617  
US-A- 3 992 486 US-A- 4 000 216  
US-A- 4 464 513  
  
• PATENT ABSTRACTS OF JAPAN vol. 013, no.  
569 (C-666), 15 December 1989 (1989-12-15) & JP  
01 236257 A (MITSUBISHI RAYON CO LTD), 21  
September 1989 (1989-09-21)

Note: Within nine months from the publication of the mention of the grant of the European patent, any person may give notice to the European Patent Office of opposition to the European patent granted. Notice of opposition shall be filed in a written reasoned statement. It shall not be deemed to have been filed until the opposition fee has been paid. (Art. 99(1) European Patent Convention).

**EP 1 022 115 B1**

**Description****BACKGROUND OF THE INVENTION****Field of the Invention**

**[0001]** The present invention relates to polymeric articles having a textured surface and frosted appearance and to resins for producing such articles.

**Related Art Statement**

**[0002]** In lighting applications, and point of purchase, and cosmetic/decorative markets, people are always looking for new and innovative products that can provide flexibility for designs and fabrications at a competitive cost.

**[0003]** Presently, there is not a successful plastic product in this market that can be used in a one-step process and provide the properties and appearance needed to replace sand blasted glass material. It would be desirable to have a resin that could be used for sheet and profile extrusion applications and that creates a product with a surface texture and frosted appearance.

**[0004]** Such a plastic material could reduce the production and fabrication costs and provide design flexibility for end users. Similar thermoplastic products are traditionally made by surface treatment, such as, sand blasting and surface pattern fabrication, and by adding inorganic filler, such as, barium sulfate, calcium carbonate, titanium dioxide, silica, etc. Such inorganic fillers are normally difficult to disperse evenly in polymer matrix material, reduce greatly the light transmission of the polymer, and do not generate the desired surface texture. Also, the filler particles have a tendency to deteriorate physical properties of the polymer.

**[0005]** Fine particles (i.e. less than 15 micrometers) of a copolymer made by an emulsion polymerization process are sometimes added into a plastic matrix to generate a light diffusion effect for display and light panel applications, for example, US patent 5,346,954. However, this type of product tends to soften the polymer matrix and cannot produce the textured surface so often preferred by the end user.

**[0006]** US 3,345,434 describes a method for the production of articles of manufacture having a rough finish which diffuses light which comprises blending particles of a crosslinked thermoplastic polymer with a second thermoplastic non-crosslinked polymer and subjecting the resultant blend to a polymer fabrication procedure.

**[0007]** EP-A-0596290 describes the use of mixtures comprising (A) from 80 to 99% by weight of a polymer based on methyl methacrylate, (B) from 20 to 1% by weight of a particulate polymer having a particle size in the range from 1 to 50  $\mu\text{m}$  which is obtainable by polymerization of a monomer which contains vinyl groups, and (C) from 0 to 60% by weight, based on (A) and (B), of a multistage graft rubber based on an ester of acrylic acid or on butadiene, for the production of rough coating compositions.

**[0008]** US 3,992,486 describes a process for preparing minute, generally spherical crosslinked polymer particles insoluble in olefinic monomers, the particles being below about 30 microns in diameter and, more specifically, particulate polymers of ethylenically unsaturated monomers and polyfunctional crosslinking monomers. The particulate polymers are said to be useful in coatings and as components of polymeric compositions as superior substitutes for conventional pigments.

**SUMMARY OF THE INVENTION**

**[0009]** The present invention provides an extruded polymeric article comprising a polymeric matrix and polymeric particles which are substantially spherical, highly crosslinked, have a mean particle size of 25-55 micrometers and have a particle size distribution between 10-110 micrometers, wherein the article has a frosted and surface textured finish, wherein the frosted appearance is achieved through the mismatch of the refractive indices of the polymeric particles and polymeric matrix by greater than 0.02, and wherein the polymer used as the polymeric matrix is an acrylic polymer and the polymeric particles comprise 10-50% styrene, 90-50% methyl methacrylate and 0.1-2.5% crosslinking agent.

**[0010]** Since the article is a thermoplastic material, it can be recycled, re-extruded, or injection molded to generate the desired appearance.

**[0011]** The purpose of the highly crosslinked spherical particles in the present invention is to impart to the thermoplastic composition a textured surface and a frosted appearance. The frosted appearance of the thermoplastic compositions is achieved through the mismatch of the refractive indexes,  $\Delta n > 0.02$ , of the fine particles and thermoplastic matrices. The surface texture is controlled by the degree of crosslinking and mean size of the fine particles.

**[0012]** Another aspect of the invention is an extrudable resin comprising

- a) 20-90% polymethyl methacrylate based matrix;  
 b) 5-50% modifiers; and  
 c) 5-30% highly crosslinked spherical beads comprising  
     10-50% styrene;  
     90-50% methyl methacrylate; and  
     0.1-2.5% crosslinking agent,

wherein the beads have a mean particle size of 25-55 micrometers, and a particle size distribution of between 10-110 micrometers, wherein there is a mismatch of refractive indices of the highly crosslinked spherical beads and polymethyl methacrylate based matrix by greater than 0.2. This resin may be used to produce the article of the invention.

[0013] In another embodiment, the invention provides an extrudable resin comprising

- a) 70-85% polymethyl methacrylate based matrix; and  
 b) 15-30% highly crosslinked spherical beads comprising  
     15-35% styrene;  
     65-85% methyl methacrylate; and  
     0.5-1.5% allyl methacrylate,

wherein the beads have a mean particle size of 25-55 micrometers, and a particle size distribution of between 10-110 micrometers, wherein there is a mismatch of refractive indices of the highly crosslinked spherical beads and polymethyl methacrylate based matrix by greater than 0.2. This resin may also be used to produce the article of the invention.

#### DETAILED DESCRIPTION OF THE INVENTION

[0014] An acrylic polymer, more preferably an impact modified acrylic polymer, is used as the polymeric matrix.

[0015] The term "acrylic polymer(s)" as used herein means

- 1) alkyl methacrylate homo polymers,
- 2) copolymers of alkyl methacrylates with other alkyl methacrylates or alkyl acrylates or other ethylenically unsaturated monomers,
- 3) alkyl acrylate homo polymers, and
- 4) copolymers of alkyl acrylates with other alkyl acrylates or alkyl methacrylates or other ethylenically unsaturated monomers.

[0016] The alkyl group can be from 1-18 carbon atoms, preferably 1-4 carbon atoms. Preferred are polymethyl methacrylate based matrix and copolymers of methyl methacrylate with from about 0.1 - 20% alkyl acrylates, wherein the alkyl contains 1 - 4 carbon atoms, alkyl acrylic acids wherein alkyl contains 1 - 18 carbon atoms.

[0017] Preferably the thermoplastic matrix material comprises a polymer or copolymer of methyl methacrylate (MMA); typical copolymers include 80 to 99% MMA and 1 to 20%, preferably 1 to 5%, of (C1-C10) alkyl acrylates, such as methyl acrylate and ethyl acrylate (EA). A suitable commercially available poly(methyl methacrylate) type thermoplastic matrix material is Plexiglas® V-grade molding powder, such as Plexiglas® V(825), V(825)HID, V(045), V(052) and V(920) etc.

[0018] The polymer matrix is conveniently prepared by conventional cell casting or melt extrusion processes and is typically provided in particulate form. In addition, thermoplastic matrix materials may be prepared by a conventional bulk process (for example, a continuous flow stirred tank reactor (CFSTR) process), solution, suspension or emulsion polymerization techniques, in which case conventional isolation processes used to recover the polymer in particulate form include, for example, filtration, coagulation and spray drying.

[0019] The matrix may also include other modifiers or additives which are well known in the art. For example, the composition may contain impact modifiers, external lubricants, antioxidants, flame retardants or the like. If desired, ultraviolet stabilizers, flow aids, metal additives for electronic magnetic radiation shielding such as nickel coated graphite fibers, antistatic agents, coupling agents, such as amino silanes, and the like, may also be added.

[0020] One of the processes of incorporating the modifier is to make the modified matrix by an emulsion process.

[0021] A rubber modifier can be added to the matrix, especially an acrylic polymer matrix, to enhance its performance properties.

[0022] In an emulsion process, particles generated are usually small, 0.05 - 5 micrometers. Initiators used for the emulsion process are water soluble. The final product from an emulsion process is a stable latex which is normally not suitable for filtration. The latex emulsion is typically spray dried or coagulated/wash dried.

[0023] The emulsifying reagents are well known to those skilled in the art. Useful emulsifying agents include common soaps, alkyl benzenesulfonates, such as: sodium dodecyl benzenesulfonate, alkylphenoxypolyethylene sulfonates, sodium lauryl sulfate, salts of long chain amines, salts of long-chain carboxylic and sulfonic acids, etc. In general, the emulsifier should be compounds containing hydrocarbon groups of 8-22 carbon atoms coupled to highly polar solubilizing groups such as alkali metal and ammonium carboxylate groups, sulfate half ester groups, sulfonate groups, phosphate partial ester groups, and the like.

[0024] The blend of the multi-stage polymer(rubber modifiers) with the thermoplastic polymer can be accomplished by any known method, such as dispersing the multi-stage polymer in a monomer mixture used to prepare the thermoplastic polymer or in a monomer-polymer syrup mixture which together would provide the desired thermoplastic polymer. Alternatively, the multi-stage polymer can be placed in a casting mix in the form of an emulsion, suspension or dispersion in water or in an organic carrier; the water or organic carrier can then be removed before or after casting into the final thermoplastic polymer form. The multi-stage polymer may also be blended with the thermoplastic polymer by extrusion compounding. Additional specific methods and details of blending the thermoplastic polymer and impact modifiers are disclosed in U.S. patent No. 3,793,402.

[0025] A preferred thermoplastic matrix material is impact modified poly(methyl methacrylate) commercially available as Plexiglas® DR101, MI-4, and MI-7 molding powder. Plexiglas® in North and South America, and Oroglas® in Europe and Asia are trademarks of Elf Atochem North America, Philadelphia, PA, USA.

[0026] The matrix material can be made by many different processes known in the art, including, continuous cell casting, emulsion, suspension, bulk polymerization, and continuous stirred tank reactions (CFSTR), etc. Each of these methods utilize free radical polymerization chemistry. In the continuous cell casting process of acrylic resins, the viscous polymer/monomer mixture, often referred to as syrup and which has about 30-50% polymer conversion, is fed between two stainless steel belts at a controlled temperature. Polymer conversion is completed with the continuous moving belt. In an emulsion process, the major components are monomers, water, emulsifiers, water soluble initiators, and chain transfer agents. The water-to monomer ratio is controlled between 70:30 and 40:60. A core/shell particle structure can be achieved through grafting by an emulsion process, which is often a preferred process for making impact modifiers.

[0027] The highly crosslinked particles may be made by a suspension process.

[0028] Crosslinking monomers suitable for use as in the spherical polymer particles (beads) are well known to those skilled in the art; and are generally monomers copolymerizable with monomers present, and having at least two or more unsaturated vinyl groups which have approximately equal or different reactivities, such as, divinyl benzene, glycol di- and tri-methacrylate and acrylates, ethylene glycol dimethylacrylate, allyl methacrylates, diallyl maleate, allyl acryloxypropionates, butylene glycol diacrylates, etc. Preferred crosslinkers are ethylene glycol dimethacrylate, divinylbenzene, and allyl methacrylate. Most preferred is allyl methacrylate.

[0029] "Highly crosslinked" means that the particulate material can not be dissolved at all in a strong organic solvent, such as tetrahydrofuran (THF) or methylene chloride(MDC). The swell ratio measurement, which measures the particle size change in an organic solvent after a certain period of time, is normally a test method to determine the degree of crosslinking. A low swell ratio, no soluble fraction in a MDC/THF solvent, and the retention of particle integrity are the indications of a highly crosslinked acrylic polymer. The degree of crosslinking can also be monitored through surface hardness and surface gloss measurements. The related test methods are American Standard Test Methods: ASTM D785 and ASTM D2457.

[0030] The beads have a mean particle size of 25-55 micrometers, and a particle size distribution of between 10-110 micrometers. The particle size may be controlled by agitation speed, reaction time, and level and type of suspending agents. The "mean particle size" is a weight mean. As used herein and in the following sections and appended claims, the term "weight mean" or "weight percent" means average by weight or the percent by weight of each component based on the total weight of composition. The light scattering methods used for particle size determination are ASTM: D4464, B822, and ISO13321:1996(E).

[0031] The composition of the polymer particles may be analyzed by a pyrolysis GC/MS spectrometer where the polymer material is pyrolyzed at an elevated temperature and the decomposed components are analyzed further for a quantitative determination.

[0032] In order for the article produced by the blend of the resin and particles to be frosted, the refractive index of the crosslinked particles has to be different from that of the matrix material. The difference in refractive index should be  $\Delta n > 0.02$ . The crosslinked spherical particles have mismatched refractive indices with many thermoplastic polymers, such as, but not limited to, acrylic polymers(defined as above), polycarbonate, polyvinyl chloride and the like, polystyrene, PET, PETG, imidized polymers of methyl methacrylate, copolymer of acrylonitrile and styrene, and copolymer of styrene and MMA.

[0033] The spherical particles may be made by a suspension process wherein the water is a continuous phase serving as a heat transfer medium and the polymerization is carried out in monomer droplets. In a suspension process the viscosity change during the polymer conversion is very small; therefore, the heat transfer is very efficient. The agitation speed, and composition and level of the suspending agent are critical factors in determining the particle size

distribution. The typical particle size from suspension is about 10 - 1000 micrometers. More detailed information about the suspension process can be found in US Patent 5,705,580, EP 0,683,182-A2, and EP 0,774,471-A1. Typical examples of using the suspension process for the spherical particles are provided in Examples 1, 2A, 2B, and 2C respectively.

[0034] It is within the scope of the present invention to color the crosslinked beads during the suspension process. The advantages of using colored beads over a colored matrix material are process flexibility, cost reduction, better color dispersion, reduced surface gloss, deep/natural color appearance and a reduction in cleaning process equipment between product changes.

[0035] A particularly preferred embodiment of the surface textured and frosted article of the present invention has the composition

- a) 70 - 85% polymethyl methacrylate based matrix; and
- b) 15 - 30% highly crosslinked spherical beads comprising
  - 15 - 35, preferably 24.9 % styrene
  - 65 - 85, preferably 74.0 % methyl methacrylate, and
  - 0.5 - 1.5, preferably 0.9 % allyl methacrylate.

[0036] The article of the present invention is produced by extrusion compounding together the crosslinked particles (beads) made from the suspension process, the optional modifiers, and the polymer matrix on a single or twin screw extruder to produce an article having a surface textured and frosted appearance.

[0037] An example of the process for producing an article of the present invention is as follows:

[0038] The cross-linked spherical beads may be dried in an hot air oven before compounding into a thermoplastic matrix through, for example, a Killion® extruder equipped with a two-stage medium work screw and a vacuum venting system. A WP® twin screw extruder can also be used for the compounding. The beads, polymer, and additives are added into the extruder through different feeders on the extruder. The conveyer system for spherical beads should be a closed system to avoid safety hazards and dust hazards. The beads are fed into the Killion® extruder through a K-TRON® hopper with an auger screw by gravimetric control or by volumetric feeding control. The temperature profile which can be used for making the frosted article when the composition contains 10-35% suspension beads, made by Example 2C, and 65-90% PMMA made by a free radical polymerization process, can be as follows:

[0039] Typical process conditions for compounding extruder:

Feed Zone:	235°C
Compression Zone:	245°C
Metering Zone:	250°C
RPM(revolution per minute)	70-100

[0040] The extruded article is oven dried before further usage.

[0041] The frosted article can be further processed the same way as normal thermoplastics, such as, by profile extrusion, sheet extrusion, injection molding, and plunge molding, etc., into various final products. The product resulting from sheet or profile extrusion will have a textured surface and frosted appearance while the product resulting from injection molding will have a frosted look.

[0042] The frosted article(for example extruded sheet product) can also be produced by feeding directly the crosslinked particles with the matrix resins into a sheet extruder or injection molding machine to eliminate the compounding step. The precompounded resin is better suited for commercial applications and user friendly because direct feeding of beads requires special equipment to handle the slippery beads.

[0043] The crosslinked beads from the suspension process can also be extrusion compounded into other polymers, such as, PC, PET, PS, ABS terpolymer, ASA copolymer, HIPS, SAN, PVC, modified PVC, MBS copolymer, etc., to generate a similar effect.

[0044] Unlike other surface treated product, the frosted appearance and textured surface from this invention can be maintained through thermoforming, bending, and other post-treatments. The "textured surface" can be generated through conventional extrusion or profile extrusion equipment without the requirements of a specific patterned roll or polishing equipment, providing process flexibility for the end users.

[0045] By the term "textured surface" as used herein is meant a minimum surface roughness of 0.5 um to as high as 30 um or higher. Surface Roughness is determined by a TENCOR Alpha-step 500 surface profiler, the reference method number can be found in ASME: B46.1.1, B46.1.2, B46.1.12, ASME Y14.36. ASME is an abbreviation for the American Society of Mechanic Engineering.

[0046] One of the advantages of the current invention is that the Total White Light Transmission (TWLT) is much

higher than the similar commercial products filled by inorganic fillers, such as barium sulfate or color concentrate, to achieve a frosted appearance. For example, barium sulfate pigmented PMMA has a 47% TWLT while the frosted product of the present invention has a 84% TWLT, and both have a similar frosted appearance. The sample made from suspension beads described in Example 2C allows more light to be transmitted in lighting applications.

[0047] TWLT is measured by a Hunterlab colorimeter-D25 model, ASTM: E1331 and E1164. The frosted appearance can be determined by an opacity measurement. The higher the opacity number, the better the hiding power of the thermoplastic sample. To have a frosted appearance, the minimum opacity number should be about 10%. The loading of suspension beads and mismatch of refractive index between beads and matrix material would affect the hiding power of the sample which is measured by the opacity number. The related standard methods for these measurements are ASTM D2805-80, ASTM D589-65, TAPPI T-425, TAPPI T-519.

[0048] The composition of the current invention can be used for profile and sheet extrusion to generate final parts for lighting, signs, point of purchase and cosmetic displays, containers, home and office decorations, furniture applications, shower doors, and office doors where privacy is preserved without sacrificing loss of light.

[0049] The present invention will now be exemplified in more detail by referencing the following, non-limiting examples.

#### Example 1

[0050] The following is a typical recipe for suspension polymerization which gives a weight mean particle size of ~35 microns.

[0051] The following ingredients are mixed and reacted to form particles of P(MMA/styrene/ALMA)

Deionized Water	1772 gram
p(dimethyldiallylammonium chloride)	32 gram
NaOH	0.048 gram
NaCl	72 gram
Gelatin	2.16 gram
DI water for gelatin (90°C)	144 gram
MMA	465.5 gram
styrene	134.5 gram
ALMA	4.86 gram
butyl peroctoate	6 gram

[0052] The water phase in this recipe is composed of deionized water, p(dimethyldiallylammonium chloride), sodium hydroxide, sodium chloride, and gelatin. The organic phase is composed of styrene, MMA, allyl methacrylate, and butyl peroctoate. The p(dimethyldiallylammonium chloride) and DI water are charged into a reactor and NaOH and NaCl are added into the mix for pH modification. The target pH is in the range of 9.5-10.5. The oxygen is removed by sweeping nitrogen gas through the reactor and heating the solution to 90°C. 2.16g gelatin is dissolved into 144g DI water at 75°C in a separate container with constant agitation until complete dissolution occurs. The gelatin solution is then added into the reactor. The reactor temperature is adjusted to 80°C and the monomer mix which is composed of MMA, styrene, allyl methacrylate, and t-butyl peroctoate is charged into the reactor with an agitation of 350 RPM. The reactor is heated gradually to 90°C over 2 hrs and polymer conversion is completed in about 4 hrs. Polymer in the form of fine particles is obtained. The crosslinked beads are then centrifuged, washed, and oven dried for extrusion compounding. The resulting particles are highly crosslinked which contain 0.81% ALMA in their composition and have a weight mean size of 35 microns.

#### Example 2A

##### Preparation of Crosslinked Microbeads by a Suspension Process

[0053] The crosslinked beads with a weight mean particle size of 20-50 microns can be prepared through the following procedure and recipe:

DI H <sub>2</sub> O	245 parts
Polyvinylalcohol	5 parts



## EP 1 022 115 B1

Monomer mix:	74 parts 24.6 parts 0.8 parts 0.6 parts	methyl methacrylate styrene allyl methacrylate lauroyl peroxide
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All portions are measured by weight.

[0054] 245 parts deionized water and 5 parts polyvinyl alcohol are fed into a stirred, temperature controlled, and pressure-resistant reactor at 40°C. The reactor is deoxygenated by a nitrogen flow and stirred until the complete dissolution of polyvinyl alcohol occurs. A monomer mix described above is then fed into the reactor. The reactor is sealed under nitrogen, and pressurized at 100KPa. The mixture is heated gradually up to 110°C over 120 minutes and kept at this temperature for 15 minutes and then cooled for discharge. After centrifuging, washing, and drying, the microbeads with a weight mean of 20-30 micrometers can be separated from waste water for sample preparation.

### Example 2B

#### Preparation of Beads by Polymeric Suspending Agent

[0055] The crosslinked beads can also be prepared by using a mixture of polymeric suspending agent and pulp water generated from previous suspension process to minimize the discharge of waste water to the environment. This process improves the separation efficiency of microbeads from suspending solution and increases yields of raw materials.

Step 1: Preparation of suspending agent	
Raw materials:	
NaOH(99.0%)	48 parts
DI H <sub>2</sub> O	702 parts
AMPS	250 parts
(2-acrylamido-2'-methylpropanesulphonic acid)	0.075 parts
Potassium persulphate	
Sodium methabisulphite	0.025 parts

[0056] 48 parts by weight of NaOH and 702 parts by weight of deionized water are charged into a reactor and stirred till NaOH dissolves. 250 parts by weight of AMPS are slowly added into the reactor, and then the PH value is adjusted to between 7 and 8 by addition of either NaOH or AMPS. Remove oxygen from the reactor by nitrogen flow and heat the reactor to 50°C. Add to the reactor 0.075 parts potassium persulphate and 0.025 parts sodium methabisulphite. After 60 minutes, the reaction should be completed and 4000 parts by weight of deionized water is added into the reactor, diluting the solution to about 5.0% solids level. The prepared solution is ready to be used as the suspending agent for making microbeads in the following step.

Step 2 Preparation of Crosslinked Beads	
Raw materials:	
Deionized water	193 parts
AMPS solution from step 1	7 parts
Monomer mix(listed blow)	100 parts

MMA	74 parts
Styrene	24.95 parts
Allyl Methacrylate	0.8 parts
t-butyl peroxy-2-ethylhexanoate	0.25 parts

[0057] 193 parts by weight of deionized water and 7 parts by weight of solution from step 1 are charged into a reactor

## EP 1 022 115 B1

with agitation. Oxygen is removed from reactor by nitrogen flow. The reactor is sealed and pressurized at 100kPa and heated to 110°C in 150 minutes. The agitation speed should be maintained at 100RPM or higher. After the reaction is completed, maintain the reactor temperature at 110°C for another 15 minutes to reduce the residual monomer before cooling for discharge. The microbeads with a weight mean about 35-60 microns are separated by centrifuging, washing, and oven drying and can be used for frosted acrylic sample preparation. The waste water which contains a total dry residues of 0.62% (at 160°C), composed of 0.2% by weight suspending agent and fractions of beads smaller than a few micrometers, can be used as the suspending agent for subsequent process.

### Experiment 2C

#### Preparation of Crosslinked Beads Using Waste Water

[0058] The microbeads can also be prepared using waste water from Example 2B. The following raw materials are charged into a reactor to make the highly crosslinked particle for frosted acrylic sample preparation.

Waste water(from example 2B)	300 parts
Monomer mix	100 parts

Composed of:	74 parts MM
	24.6 parts styrene
	0.8 parts ALMA
	0.6 parts lauroyl peroxide

[0059] Introduce 300 parts of waste water from example 2B into a pressurized reactor and heat to 80°C and then introduce 100 parts of monomer mix into the same reactor with continuous stirring. Remove the oxygen from the reactor by a nitrogen flux. Pressurize the reactor at 100Kpa and seal. Heat the reactor gradually to 110°C in 150 minutes. After complete conversion, the reactor temperature is maintained at 110°C for another 15 minutes and then cooled down for discharge. Microbeads with a weight mean particle size of 50 microns are separated from the solution by centrifuging, washing, and oven drying.

### Example 3

[0060] In order to evaluate the compositional effect of different particles in thermoplastic matrixes, samples are made by the following method for evaluation of their appearance, transmission light efficiency, and surface texture effect.

[0061] The EX III-A sample is made by compounding 25% suspension beads which have a composition of 74.3% methyl methacrylate, 24.8% styrene, and 0.9% allyl methacrylate, into 75% of an impact modified PMMA matrix (MMA/BA/Styrene/ALMA) on a Killion® extruder equipped with a medium work two stage screw and a vacuum vent for monomer/moisture removal.

[0062] The EX III-B sample (Comparative Example) is made by compounding 25% suspension beads which have a composition of 79.3% methyl methacrylate, 19.8% butyl acrylate, and 0.9% allyl methacrylate, into 75% of an impact modified PMMA matrix (MMA/BA/Styrene/ALMA) on a Killion® extruder.

[0063] The EX III-C sample (Comparative Example) is made by compounding 20% inorganic beads, Scotchlite Glass Bubbles sold by 3M, into 80% of an impact modified PMMA matrix (MMA/BA/Styrene/ALMA) through a Killion® extruder.

[0064] The samples used in this example are made through a two step extrusion process: compounding the different particles with impact modified PMMA matrix to make a resin; and passing the resin through a sheet extruder to make 3.2 mm (0.125") thickness sheet for testing. The temperature profiles used for resin compounding and sheet extrusion are listed in the following table:

#### Resin compounding conditions

[0065]

Feed Zone	Compression Zone	Metering Zone	Die Zone	RPM
235°C	245°C	250°C	275°C	85

## EP 1 022 115 B1

### Sheet Extrusion Conditions

[0066]

5

Feed Zone	Compression Zone	Metering Zone	Die Zone	RPM	Roll temp.
225°C	240°C	240°C	260°C	85	82°C

10

15

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25

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35

40

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55

Sample	Wt % load	Bead type	Mean particle size <sup>1</sup>	Appearance	Total white light transmission (TWLT) <sup>2</sup>	Surface roughness <sup>3</sup>
ExIII-A	25	crosslinked Sty/MMA/ ALMA	31.8	translucent/ textured surface	83.5%	9.6 um
ExIII-B	25	crosslinked BA/MMA/ ALMA	57.1	white agglomerate /turbid texture surface	78.9%	4.3um
-ExIII-C	20	Inorg.glass beads	55	Opaque/ proc. problem./ brittle incompatible	N/A	N/A

<sup>1</sup> Light scattering method was used to determine weight mean particle size.

<sup>2</sup> TWLT was measured by a Hunterlab colorimeter-D25 model, ASTM:E1331 and E1164

<sup>3</sup> Surface Roughness was determined by a Tencor® Alpha-step 500 surface profiler, ASTM:method B46.1.1, B361.2, and Y14.36.

Conclusions: The suspension beads of EX III-A give the best result for frosted resin. It is easier to disperse the suspension particles of EX III-A than the other two compositions, EX III-B and EX III-C, in a thermoplastic matrix. Although the glass beads in EX III-C has a similar particle size range, it can not generate the desired surface texture and light transmission efficiency. The glass beads are not compatible with the thermoplastic material at higher loadings and deteriorate the polymer's physical properties. The parts made in EX III-C are very brittle and can not pass the visual test.

#### Example 4

[0067] The following table shows the results of using the crosslinked spherical particles made by the method of Example 2C for other thermoplastic matrixes. The sample appearance, the surface roughness, and the total white light transmission are measured for different samples. The samples are made by extrusion compounding the crosslinked beads with PVC (Comparative Example), PC (Comparative Example), Polystyrene (Comparative Example), and PMMA polymer material in a 20% suspension particles and 80% polymer matrix material on a Killion® extruder with a two stage medium work screw and a vacuum vent. The resins are then passed through a sheet extruder.

[0068] The following conditions are used for sample preparation:

#### Temperature Profile for Extrusion Compounding

[0069]

	Feed Zone	Compression Zone	Metering Zone	Die Zone	RPM
PVC-1	182°C	182°C	182°C	182°C	100
PC-1	249°C	271°C	265°C	265°C	80
PSY-1	238°C	238°C	243°C	243°C	100
PMMA-1	220°C	230°C	235°C	240°C	100

[0070] The sheet extrusion conditions for each of the samples are listed in the following table:

#### Temperature Profile for Sheet Extrusion

[0071]

	Feed Zone	Compression Zone	Metering Zone	Die Zone	RPM	Roll Temp
PVC-1	182°C	182°C	182°C	193°C	100	82°C
PC-1	249°C	260°C	260°C	265°C	80	82°C
PSY-1	226°C	232°C	232°C	232°C	100	82°C
PMMA-1	210°C	225°C	230°C	240°C	100	82°C

[0072] The sample for the Surface Roughness Measurement is made by sheet extrusion at a 3.2 mm (0.125") thickness and the sample for total white light transmission(TWLT) is made by an injection molding machine with the same temperature profile as sheet extrusion conditions. The mold temperature as listed in the following: PVC-1 at 65.5°C ; PC-1 at 71°C; PSY-1 at 60°C; PMMA-1 at 65°C.

[0073] Conclusion: The copolymer beads made by a suspension process can be used for different thermoplastic matrixes at a 5-35% loading. All of the samples give a frosted, non gloss appearance, and textured surface, and the samples maintain good physical properties. The PMMA-1 sample gives a better light efficiency and surface texture. It is noted that the loading of the beads in polycarbonate should be lower in order to have better light transmission. All the samples have good hiding power, high light output and low object recognition.

[0074] The compositions all use 20% beads of 74.3% MMA/24.8% Styrene/0.9% ALMA and have a weight mean particle size of 57 micrometers. The beads were made as in Example 2C.

Frosted Matrix Polymer Data

[0075]

Matrix polymer	Total white light transmission (TWLT) <sup>2</sup>	Surface roughness <sup>3</sup>	Sample Appearance
PVC	77.1%	13.5 um	textured Translucent
PC	28.9%	4.3 um	textured Translucent
P-Styrene	56.4%	15.5 um	textured Translucent
PMMA <sup>1</sup>	85.7%	12.8 um	textured Translucent

1- Matrix polymer has a composition of 96%MMA/4%EA.

2- TWLT-total white light transmission is determined by a Hunterlab colorimeter and the ASTM method is E1331 and E1164.

3- Surface Roughness is determined by a Tencor® Alpha-step 500 surface profiler and the ASTM method is B46.1.1, B361.2, and Y14.36.

Example 5Effect of Different Concentrations of Styrene/MMA/ALMA Crosslinked Beads in PMMA Matrix

[0076] This experiment is designed to evaluate the concentration effect of the particles on the final product's surface texture, total light transmission, appearance, hiding power, and mechanical impact properties. The surface roughness measurement is made on a TENCOR Alpha-step 500 surface profiler. The appearance is evaluated visually. The total light transmission is a measurement of lighting efficiency. The Melt Flow Rate, used broadly by the those skilled in the art, gives the process flow information for the sample. The Dynatup impact test is used for mechanical impact properties.

[0077] In order to understand the best loading level of spherical particles made by the suspension process, samples are prepared by the sheet extrusion and injection molding methods using a rubber modified PMMA matrix (MMA/EA/BA/Styrene). The suspension beads are compounded into the rubber modified matrix material through a Killion® extruder equipped with a two stage medium work screw at the following conditions:

Feed Zone	Compression Zone	Metering Zone	Die Zone	RPM
225°C	235°C	235°C	240°C	100

[0078] The resin is then injection molded into parts, as known to those skilled in the art, for the analysis of light transmission, mechanical properties, and extruded into sheet sample at 3.2 mm (0.125") thickness for surface texture analysis.

Sample ID	Bead conc. % <sup>1</sup>	Dynatup <sup>2</sup>	Appearance	Surface roughness	Total Reflect light	Total white light transmission (TWLT)	MFR <sup>3</sup>
FST-0	0	11.3 J (8.3 ft-lb) <sup>4</sup>	Clear/ gloss	0.128um	7.41%	90.4%	1.76
FST-5	5	9.88 J (7.29ft-lb)	Gloss/ Transparent	4.36um	7.46%	88.9%	1.23

1- The composition of the beads is 74.3%MMA/24.8%styrene/0.9%ALMA. The amount of crosslinking is 0.9%(particle is highly crosslinked) and weight mean particle size is 48 micrometers. The beads were made as in Example 2B.

2- Impact Strength is determined by a Dynatup impact tester (Model SFS), made by General Electric Research (ASTM D3763)

3- MFR is an abbreviation of melt flow rate (ASTM D-1238, at 230 degree C, 3.8kg),condition "I" and procedure "A"

4- The significance of sample FST-0 with 0% beads having a 11.3 J (8.3 ft/lb) ISFD while sample FST-20 with 20% beads having a 7.73 J (5.7 ft/lb) ISFD is that standard PMMA polymer without rubber modification has an impact strength (Dynatup method) of 1.36 J (1.0 ft/lb), and rubber modified PMMA polymer has a falling dart impact strength of 11.3-13.6 J (8.3-10.0 ft/lb). Thus, the sample having 20% beads still has a very high